

Article

The Effect of the Hydraulic Retention Time on the Performance of an Ecological Wastewater Treatment System: An Anaerobic Filter with a Constructed Wetland

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Academic Editor: Say-Leong Ong

Received: 18 December 2014 / Accepted: 19 February 2015 / Published: 17 March 2015

Abstract: This work assesses the performance of a municipal pilot wastewater treatment system employing an up-flow anaerobic filter (UAF) followed by a horizontal subsurface constructed wetland (HSSCW). This pilot scale demonstration project was implemented in a zone with subtropical climate in order to protect Lake Chapala from wastewater loads that are discharged by small communities in the Lake's vicinity. The filters were filled with tezontle as the media for biofilm support and the HSSCW was planted with two ornamental plants species, *Canna hybrids* and *Strelitzia reginae*. The experiment evaluated three hydraulic retention times (HRT) of 18, 28 and 38 h in the UAF, which corresponds to two, three and four days in HSSCW over 66 weeks. The mean efficiencies found for the complete system were 80% and 90% of BOD, 80% and 86% of COD, 30% and 33% of N_{tot} and between 24% and 44% of P_{tot} . It was possible to remove almost 80% of organic matter in 18 h in the UAF while the HSSCW reached 30% of removal for N_{tot} in a HRT of three days. As expected, the UAF was responsible for removing most of the organic matter and the HSSCW removed most of the nitrogen.

Keywords: constructed wetland; up-flow anaerobic filter; organic matter removal; nutrient removal; hydraulic retention time (HRT)

1. Introduction

Untreated wastewater discharged by cities and small rural communities contains nutrients that alter lakes and streams by accelerating the eutrophication process and thus change the quality of freshwater bodies [1–3]. A convenient ecological alternative that works well for small rural communities is to treat the municipal wastewater through constructed wetlands [4,5].

An artificial or constructed wetland is a natural treatment system designed and constructed to imitate hydrodynamic mechanisms as well as biogeochemical pollutant degradation processes that occur in natural wetlands, but with a greater degree of control over the hydraulic regime of the system [6]. The goal is to improve the quality of an effluent by optimizing the treatment systems [7]. A horizontal subsurface flow constructed wetland (HSSCW) includes low depth excavations or channels, emergent vegetation planted on a layer of soil of a porous or granular media that allows for the horizontal subsurface flow of the effluent. The permeable bed (formed by the granular media, the rhizomes and plant roots) is elevated and the water level is below the surface of the bed. Construction includes the placement of a plastic membrane for groundwater and soil protection and adequate inlet and outlet hydraulic structures to control water level [8–12]. Low energy requirements, easy operation and maintenance, modest installation and maintenance costs, minor sludge production, and the creation of a visually pleasing landscape are some advantages of this technology [5,13,14]. The clogging of granular media is one of the main operation problems in subsurface flow constructed wetlands [15]. It is linked to media type and it, in turn, is linked to hydraulic retention time since the hydraulic conductivity of porous media is very sensitive to media size and is influenced by particle size distribution and particle shape [16]. An adequate selection of granular media could decrease the estimated wetland area and improve the removal efficiencies [4,17].

Constructed wetlands are commonly used for secondary treatment in small communities [8]. However, they need a large land area [18] and therefore, it is sometimes necessary to add a previous treatment stage to the natural treatment system [18,19]. Anaerobic processes are a treatment technology that can be effectively integrated with constructed wetlands because they require a very small input of energy, minimum investment and operational costs, generate less biosolids when compared to conventional aerobic systems, and they can prevent clogging [15,18,20,21]. The up-flow anaerobic filter (UAF), as part of this technology, is able to treat wastewater with different pollutant loadings and it is successfully used, specifically for small communities in warm climates, to achieve the desired water quality. In general, the UAF removes dissolved and suspended solids through close contact with anaerobic bacteria attached to the filter media [22,23].

Both the wetlands and UAF wastewater treatment processes have been individually studied with good results. The UAF removes mainly organic matter in wastewater with low and high organic loads, while the HSSCW is capable of removing organic matter and nutrients and is commonly used to obtain secondary or tertiary effluent concentration levels [8,23–25]. In other words, combining an anaerobic

reactor with a constructed wetland brings important benefits to the constructed wetlands system, such as the reducing of the required planted area, reducing of the retention time, and increasing of their life cycle [18,20]. Few studies have been conducted on this coupled treatment process.

The aim of this study was to determine the effect of the hydraulic retention time on the performance of the coupled treatment system, integrated with an up-flow anaerobic filter and a horizontal subsurface constructed wetland, operated under subtropical climate conditions. Moreover, it was to evaluate the constructed wetland efficiency considering its area reduction. Provisions were included that allowed the control of the hydraulic retention time (HRT) to assess the impact on the reduction of organic matter and nutrients.

2. Materials and Methods

2.1. Treatment System Description

The pilot-scale constructed wetland was built on the site of the municipal wastewater treatment plant for Chapala, Jalisco, Mexico. This town is located on Lake Chapala (20°07'–20°21' N and 102°40'45"–103°25'30" W) at an altitude of 1524.6 m above sea level. This area has a semi-warm sub-humid climate with summer rain, dry and semi-warm winters and springs. According to Köppen–Geiger climate classification, it is defined as a subtropical humid climate (Cwa) making this proposal possible in this type of climate around the world [26,27].

Wastewater was diverted from the grit removal chamber at the wastewater treatment plant. Raw wastewater was pretreated with a UAF with a filling height of 90% and with the dimensions of 1.75 m deep, 4 m long and 2.3 m wide. UAF effluent flowed to the HSSCW with the dimensions of 0.6 m deep, 9.2 m long and 7.6 m wide. The system was designed to operate with a water flow rate of 11 m³·day⁻¹, in order to provide for 110 person equivalents (PE). Both, the UAF and the HSSCW use tezontle as biofilm support. Tezontle is the Indian name of a volcanic red-orange extrusive rock classified as part of the feldspar family. This material has a high porosity (up to 65% pore volume for grain size of 20–25 mm), and this characteristic gives it a high surface area to volume ratio (390 m²·m⁻³) compared to synthetic media (164 m²·m⁻³). It has been tested and used in a number of environmental applications [28], and it is inexpensive, since it is abundant in Mexico [29]. Furthermore, the material is considered inert, with pH values close to neutral, low cation exchange capacity, good ventilation and capacity in humidity retention depending on particle diameter [30]. While the UAF contains tezontle of 1 inch diameter, the HSSCW was backfilled with two layers: The first with 50 cm of tezontle of 1 inch diameter and the second with 10 cm of tezontle of 0.25 inch diameter. The porosity of clean tezontle, tested prior to the experiments was determined to be 58% (1 inch) and 60% (0.25 inch), respectively. As part of the construction, an impermeable plastic liner of 1 mm thick HDPP (High Density Polypropylene) was installed at the bottom of the treatment unit to prevent groundwater contamination. In addition, an adjustable outlet was installed at the end of the bed, which permitted better water level control. The HSSCW was planted with two plant species, the first half with *Canna hybrids* and the second half with *Strelitzia reginae*. Around one hundred plants from each species were planted in a geometric pattern of quincunx with a distance of 0.5 m between each plant of *Canna hybrids* and 0.55 m between each *Strelitzia reginae*, which provided an initial plant density of three plants per m². The warm climate enables

the use of non-conventional species; Zurita *et al.*, (2009) suggest that it is possible to produce commercial flowers in constructed wetlands without reducing the efficiency of the treatment system. Therefore, these plants can acclimate well and grow, and also give a pleasing appearance [29,31].

2.2. Treatment System Monitoring

Once construction was completed, a start-up period of six months was used before beginning the monitoring stage in order to ensure greater plant coverage, which suggests a stable performance for pollutant removal [32], since it provides microorganisms the opportunity to grow and to adhere to the surface roots of the planted species and to the solid-porous substrate. Figure 1 shows the cover plant in the constructed wetland.



Figure 1. Wastewater Treatment System (field view).

Monitoring was conducted for 66 weeks, divided into three periods, to test the following hydraulic retention times: HRT1 corresponds to 18 h in the UAF and two days in the HSSCW, HRT2 was for 28 h in the UAF and three days in the HSSCW, and HRT3 was for 48 h in the UAF and four days in the HSSCW. In HSSFCW, the hydraulic retention time can vary between three and fifteen days to achieve an adequate treatment depending on pollutants to be removed [33]. Shorter retention times were chosen in order to test the response of the constructed wetland performance considering the previous addition of an anaerobic filter. The samples were collected weekly at four monitoring points along the treatment system (Figure 1): Influent (M1), outlet UAF/inlet HSSCW (M2), middle part of HSSCW (M3) and effluent (M4). For sampling points M2 and M4 (constructed wetland stage) it is important to point out that the first part of HSSCW was planted with different ornamental plants than the second stage. The sampling point M3 marked the separation between the two ornamental plants used. *Strelitzia reginae* was placed in the second part of the HSSCW because it has been proven that *Canna hybrids* adapt better to these conditions, showing high growth rates [31,34].

2.2.1. Water Quality Analysis

Water samples were taken to measure five-day biochemical oxygen demand (BOD), chemical oxygen demand (COD), total nitrogen (N_{tot}), ammonia nitrogen ($\text{NH}_4\text{-N}$), nitrite (NO_2), nitrate (NO_3) and total phosphorous (P_{tot}). The analytical methods used for the water quality analyses were in accordance with

“Standard Methods for the Examination of Water and Wastewater” [35]. Total inorganic nitrogen was estimated as the sum of $\text{NH}_4\text{-N}$, NO_2 and NO_3 . Some parameters were measured in the field, including Electrical conductivity (EC), pH (waterproof PC 300 hand-held pH/conductivity/TDS/Temperature meter OAKTON[®], Vernon Hills, IL, USA), temperature (Temp.), relative humidity (RH) (4184 Traceable[®], Jumbo Humidity/Temperature meter Friendswood, TX, USA) and dissolved oxygen (DO) (YSI 58 DO meter, Yellow Springs, OH, USA) in the constructed wetland with at a depth of 20 cm below the water table.

2.2.2. Statistical Analyses

A statistical model was utilized to determinate how pollutant concentration varied between sampling points and for different HRT. Data was assessed with a Nested Design with a crossover factor using Statgraphics Centurion XVI[®] (Warrenton, VA, USA) with a confidence level of 95% [36]. The experiment was designed to compare the response (pollutant concentration) relative to categorical factors, including sampling points, HRT and time.

3. Results and Discussion

3.1. In-Situ Field Conditions

The major parameters that influence the removal mechanisms for nitrogen and organic matter in constructed wetlands are pH, dissolved oxygen (DO) and temperature [17]. This is because organisms present in biological wastewater treatments are sensitive to these parameters. Table 1 shows the mean values and standard deviations for temperature, RH and pH. The UAF stage of the process is represented by sampling points M1 (influent) to M2 (effluent), while the HSSCW stage is between sampling points M2 (influent) and M4 (effluent). A significant difference ($p \leq 0.05$) between treatment stages was observed for pH, but the DO did not show a significant difference between the sampling points M3 with a mean value of $0.71 \text{ mg}\cdot\text{L}^{-1}$ (± 0.2) and M4 with a mean value of $0.8 \text{ mg}\cdot\text{L}^{-1}$ (± 0.2) in the three tested HRTs.

Table 1. Mean values (\pm SD ^a $n = 40$) of temperature (Temp.) and relative humidity (RH) for environmental conditions and pH in every sampling point.

Parameter	HRT1	HRT2	HRT3	
Temp. (°C)	23.2 \pm 1.9	21.7 \pm 1.8	24.6 \pm 1.4	
RH (%)	49.8 \pm 10.5	50.3 \pm 9.8	42.9 \pm 9.4	
pH	M1	7.4 \pm 0.2	7.1 \pm 0.3	7.2 \pm 0.2
	M2	6.9 \pm 0.2	7.1 \pm 0.3	6.9 \pm 0.2
	M3	7.2 \pm 0.2	7.4 \pm 0.2	7.2 \pm 0.1
	M4	7.2 \pm 0.3	7.4 \pm 0.3	7.1 \pm 0.1

Note: ^a SD: Standard deviation.

The pH reduction at sampling point M2 is due to anaerobic conditions that are predominate in the UAF ($p \leq 0.05$). After M2, in almost all cases, a slight increase in pH was observed at the next sampling points (M3 and M4) because conditions in HSSCW are generally considered facultative. A straight-line correlation ($p \leq 0.05$) was established between inlet and outlet pH, for every stage that indicates a dependence on this parameter in the influent. In addition, the BOD removal efficiency and N_{tot} removal

efficiency of UAF showed dependence on the inlet pH ($p \leq 0.05$) with 40% and 35%, respectively, demonstrating that the efficiency of an anaerobic process depends mainly on pH [24].

The microorganisms responsible for nitrogen removal depend on temperature. The range of temperature favorable for nitrification is between 16.5 and 32 °C and for denitrification, the favorable temperature range is between 20 and 25 °C [17]. During the experiment, the recorded average temperature was 23 °C (± 2.1) and the relative humidity was 48% ($\pm 10\%$). The warm environmental conditions and the wastewater characteristics boosted the degradation of organic matter and nutrient removal.

3.2. Performance and Removal Efficiencies

Initially, organic matter decomposition is determined by the balance between organic matter load and oxygen transfer rate, which defines the predominant conditions of anaerobic and aerobic systems [9]. The organic matter, expressed as BOD and COD, is decomposed by aerobic and anaerobic microbial processes and also by physical processes, such as sedimentation and filtration. The Figure 2 shows the mean values for COD and BOD while the Figure 3a,b show all the COD and BOD data during the monitoring period. At each sampling point, the results showed a reduction across the treatment system, the BOD/COD global ratio registered was 0.52. It is possible that the UAF is responsible for the removal of most part of the organic matter (from 50% to 80%). At sampling point M2, the lowest BOD/COD ratio (0.498) was found, indicating the presence of more oxidizable species that are biodegradables. In the beginning, the monitoring plan was scheduled to assess from three to five days, but once the treatment system behavior was observed and evaluated, the retention time of five days was changed to two days as it is shown in the Figure 3.

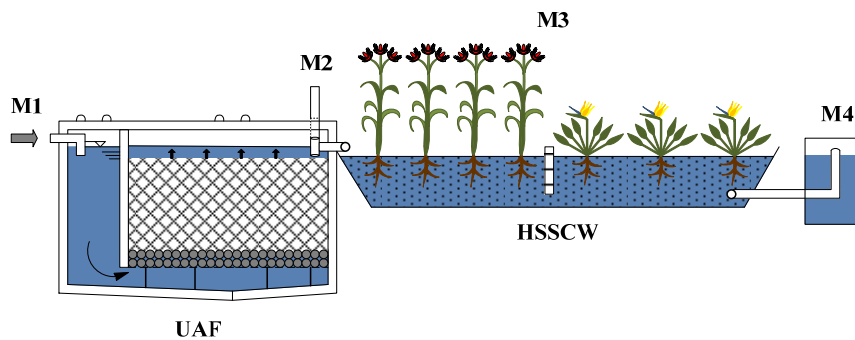


Figure 2. Sampling points in the wastewater treatment system. M1-influent; M2-outlet UAF/inlet HSSCW; M3-middle part of HSSCW; and M4-effluent.

It was observed that the greatest portion of the BOD was removed in the first half, from 42% to 53%, while the second half of the HSSCW was between 8% and 19%. This could be because the majority of the easily biodegradable BOD is removed in the first stage. The complete treatment system reached a BOD removal of 89.5%, 79.3% and 86.1% for the HRT1, HRT2 and HRT3, respectively. The COD removal values obtained were 84.2% for HRT1, 85.6% for HRT2 and 81.7% for HRT3. In the Table 2 is possible to observe the mean values for COD and BOD obtained in every sampling point and HRT. Significant differences ($p \leq 0.05$) were found between the treatment stages (evaluated in the sampling points M1, M2 and M4), and between the HRTs as followed: HRT1 and HRT2, and HRT1 and HRT3.

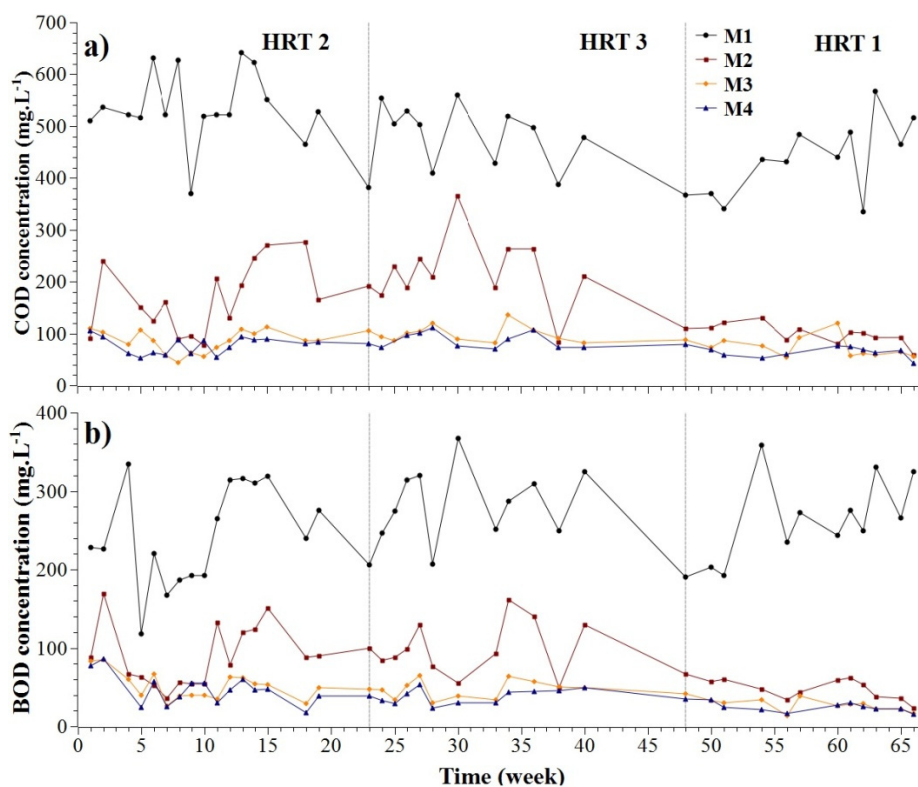


Figure 3. COD (a) and BOD (b) concentration for every sampling.

Table 2. Mean values (\pm SD, $n = 40$) of COD and BOD ($\text{mg}\cdot\text{L}^{-1}$) in every sampling point and HRT tested.

Sampling Point	HRT1		HRT2		HRT3	
	COD	BOD	COD	BOD	COD	BOD
M1	436.54 (72.42)	261.50 (54.70)	537.77 (68.81)	243.84 (63.90)	478.90 (62.68)	279.58 (49.58)
M2	98.76 (19.88)	48.73 (14.10)	167.80 (68.16)	90.35 (40.31)	217.58 (66.97)	100.25 (33.92)
M3	75.04 (21.65)	28.25 (9.06)	84.82 (21.21)	52.03 (18.01)	100.72 (16.35)	47.25 (11.45)
M4	66.86 (12.92)	25.83 (7.47)	76.88 (16.49)	47.63 (18.85)	86.25 (14.45)	38.33 (9.20)

Most of the nitrogen forms present in municipal wastewater are organic nitrogen at about 60% and ammonium at about 40% [37]. In this study, the average N_{Org} and $\text{NH}_4\text{-N}$ concentrations in the affluent (M1) of 14 ± 7 and $26 \pm 6.4 \text{ mg}\cdot\text{L}^{-1}$, respectively, were found, which corresponds to 65% and 35.5% of the total nitrogen, respectively. Nitrogen has a complex biogeochemical cycle, despite the multiple mechanisms involved, nitrogen removal is only achieved by means of denitrification, ammonia volatilization, nitrogen assimilation in vegetal tissue, sedimentation of dead plant material and ammonia adsorption to the bed [6,38]. Figure 4 shows the change of nitrogen concentration along the treatment system. The N_{Org} is converted into $\text{NH}_4\text{-N}$ by ammonification (mineralization). During this process, the organic matter is biologically degraded in aerobic and anaerobic conditions with an optimum pH range between 6.5 and 8.5 [6,38,39]. Therefore, the N_{Org} decrease along the entire treatment system with

a global efficiency of 75.7% in HRT1, 60.5% in HRT2 and 80.8% in HRT3. In the second part of HSSFCW (from M3 to M4), a small increment was found that attributed to the accumulation of detritus [6,11,39]. The next step is the nitrification process; whereby the compounds with reduced nitrogen are sequentially oxidized to nitrate with the formation of nitrite as an intermediate compound, which means that the oxygen is the terminal electron acceptor [6,39,40]. The anaerobic conditions of UAF (M2) promoted the conversion of organic nitrogen to ammonia with a result of 20.7% and 79.1% final concentrations, respectively, with a significant difference ($p \leq 0.05$), thus reducing the nitrification and the formation of nitrates. Removal of total nitrogen in UAF occurs mostly due to the reduction of nitrate under the anaerobic conditions. Besides, municipal wastewater is characterized by low concentrations of nitrates and nitrites [39]. The average nitrate concentration obtained at sampling point M1, $0.086 \pm 0.042 \text{ mg}\cdot\text{L}^{-1}$, and the average nitrite concentration, $0.022 \pm 0.007 \text{ mg}\cdot\text{L}^{-1}$, confirmed this. During the next sampling points, the nitrate continued to decrease; the mean value found at M2 was $0.037 \pm 0.024 \text{ mg}\cdot\text{L}^{-1}$, M3 $0.017 \pm 0.11 \text{ mg}\cdot\text{L}^{-1}$ and M4 $0.007 \pm 0.007 \text{ mg}\cdot\text{L}^{-1}$. Finally, the nitrate could be reduced in anoxic conditions to gaseous nitrogen by means of denitrification, which is considered the main mechanism for nitrogen removal [6,41]. In general there are significant differences between the treatment stages for N_{tot} , N_{Org} and $\text{NH}_4\text{-N}$; regarding the retention time, the N_{tot} and N_{Org} showed significant differences between HRT1 and HRT3 as well as between HRT2 and HRT3.

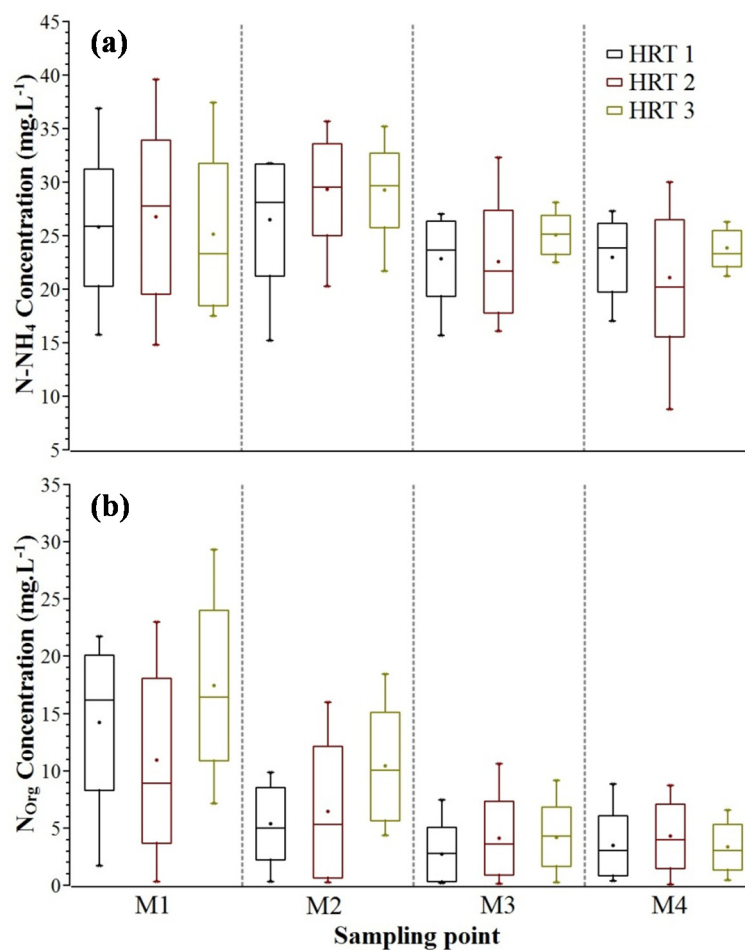


Figure 4. Plot of N-NH_4 ($\text{mg}\cdot\text{L}^{-1}$) (a) and N_{Org} ($\text{mg}\cdot\text{L}^{-1}$) (b), with maximum and minimum values and standard deviation.

When the objective is to remove nutrients from municipal wastewater, several authors report that 10 days of retention time is required [25,42] to remove any constituent. The hydraulic retention time recommended as a prescriptive scaling factor to wetland design is between 10 and 13 days [8]. In this study, the treatment system removal of nitrogen and phosphorus showed a removal efficiency of 32.5% and 43.8%, respectively, in the HRT1; 30% and 24.2% in the HRT2; and, finally, 32.9% and 30.2% in the HRT3.

Phosphorous removal is governed mainly by sorption processes on the media that is used, and phosphorus can be stored in the accumulated sediments [43]. The largest decrease of P_{tot} was observed in the UAF at sample points M1 and M2 ($p \leq 0.05$), as is shown in the Figure 5; since the retention of phosphorus in previous units is mostly due to sedimentation of particulate fraction [39]. Removal of up to 37% was measured and is attributed, primarily, to adsorption on the biofilm formed on tezontle. The biofilm begins to form by a natural process on the tezontle surface. Then, the oldest layers are detached while a newer layer is formed, and finally the biofilm settles on the bottom of the UAF. This process is repeated constantly. When the sediment reaches a determined volume, it is removed with the sludge purge where the phosphorus contained in the biofilm is removed [24].

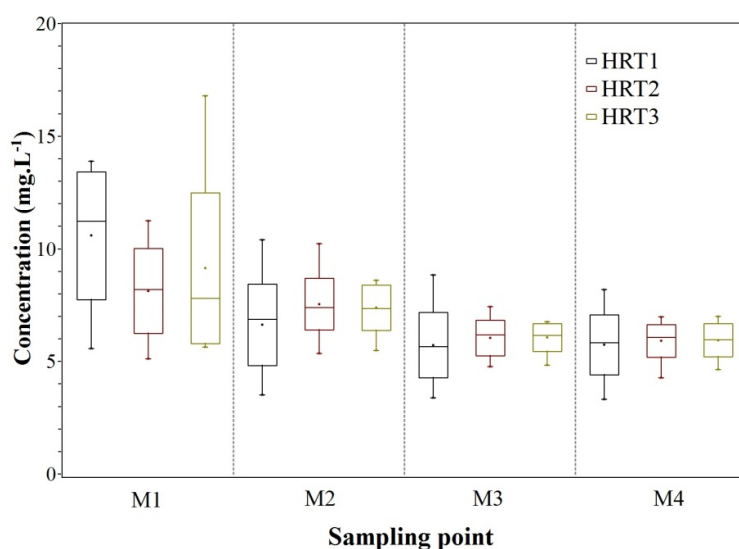


Figure 5. Plot of P_{tot} ($\text{mg}\cdot\text{L}^{-1}$), with maximum and minimum values and S.D.

The classic approach for treating wastewater from small communities has generally been with septic tanks [44]. Vymazal and Kröpfelová [39] report an average efficiency for previous treatment stages, such as septic and Imhoff tanks of 40.1% in BOD_5 , 37% in COD, 25.8% in N_{Org} , -1.8% in NH_4-N , 8.8% in N_{tot} and 10.5% in P_{tot} . Population growth and environmental conditions influence the factors used for the selection of biological wastewater treatment. The efficiency of treatment required as well as the size and cost of systems have led to implementation of new anaerobic technologies as shown in Table 3. This Table reflects the best removal efficiencies achieved by this study and compares the results with other studies where anaerobic technology treatment was used previous to a horizontal subsurface constructed wetland in order to treat municipal wastewater.

Table 3. Pollutant removal efficiency comparison (%).

Case Study	Anaerobic Treatment						Constructed Wetland (CW)						Global Efficiency				
	1	2	3	4	6	7	1	2	3	5	6	7	1	2	3	6	7
Wastewater Treatment	UAF ^a	UAF	UASB ^b	TSUAR ^c	ABR ^d	UASB	HSSCW ^e	HSSCW	HSSCW	HSSCW	SFCW ^f	SFCW	UAF	ST ^g	UASB	ABR	UASB
												HSSCW	HSSCW	HSSCW	HSSCW	SFCW	SFCW
BOD	79.8 ± 9.0	56.6 ± 2.1	63.2	70	–	44.8	38.4 ± 35.8	50.6 ± 21.7	78	79–82	–	76.6	89.5 ± 4.4	78.1	92	–	87.1
COD	76.1 ± 7.5	49.6 ± 2.6	≈61	80	30.3 ± 1.4	49.4	44.7 ± 29.5	–	78	78–82	78.1 ± 2.3	70.9	84.3 ± 4.0	81.1	91	81.2 ± 2.3	85.3
N _{tot}	23.2 ± 10.7	–	–	–	31.3 ± 1.3	–	30.0 ± 8.0	–	≈24	–	83.4 ± 2.5	–	33.0 ± 17.7	–	≈27	82.3 ± 1.9	–
P _{tot}	35.4 ± 15.5	–	35	–	34.4 ± 2.2	–	21 ± 9.9	–	38	15	61.2 ± 2.1	–	43.8 ± 12.3	–	60	67.2 ± 2.3	–
HRT (h)	18	<8	8	48	110	5.5–10	72	<24	120	8.9–9.0	7	–	–	–	–	–	–

Notes: 1 This study, 2 [44], 3 [46], 4 [49], 5 [47], 6 [45], 7 [21]; ^a UAF: Up-flow anaerobic filter, ^b UASB: Up-flow anaerobic sludge blanket, ^c TSUAR: Two-step upflow anaerobic reactor; ^d ABR: Anaerobic baffled reactor; ^e HSSCW: Horizontal subsurface flow constructed wetland, ^f SFCW: Surface flow constructed wetland, ^g ST: Septic tank.

With other anaerobic technologies, the UAF process has demonstrated a good performance for removal of organic matter and phosphorus. Nitrogen removal was slightly lower compared to the result of Ye *et al.* [45], where it used a full-scale anaerobic baffled reactor (ABR) followed by a constructed wetland with a total retention time of 124 h, with a temperature between 20 and 25 °C, an HSSFCW area of 297 m², under a hydraulic loading of 50 m³·(m²·day)⁻¹, and with the start-up phase of nine months; however, the HRT tested in the HSSFCW was nine times shorter. Constructed wetlands coupled with anaerobic treatments in these studies, had some differences with regard to the wetland type, the type of plants used, granular media, climate and the retention time or the system configuration. The BOD removal efficiency found in this study was similar to the efficiency reported by Villegas *et al.* [44], who also worked in tropical conditions, with a UAF with an HRT of 8 h while the HSSCW used an HRT shorter than one day, an area of approximately of 107 m² and a mean water flow of 1.85 ± 0.4 L·s⁻¹. While the N_{tot} removal efficiency was slightly higher in the study of El-Khateeb and El-Gohary [46], who assessed the capability of a system consisting of an up-flow anaerobic sludge blanket (UASB) reactor followed by HSSCW. This system was implemented in an arid and semi-arid zone, the HSSCW was planted with a density of three rhizomes per m², in an area of 2 m², and operated an HRT of 5 days while the UASB retention time was of 8 h, meaning a longer HRT compared to that used in the present study. The P_{tot} removal efficiency was higher than that found by El Hamuri *et al.* [47] where limestone aggregates were used as filling material. In this study the behavior of a HSSCW used as post-treatment behind a two-step upflow anaerobic reactor (TSUAR) in Mediterranean conditions is evaluated. The HSSCW had an area of 28 m², a water flow of 9.5 m³·day⁻¹ and HRT of 9 h. The global efficiencies reached for organic matter removal (up to 80%) were as expected, and they were comparable with to treatment systems with combined high rate anaerobic reactors and constructed wetlands as surface flow constructed wetlands (SFCW) with HSSCW. Better nitrogen removal has been found when constructed wetlands are combined with anaerobic treatment than for HSSCW units without a treatment stage previous. In addition, the area decrease is noticeable when the P-k-C* kinetic removal model [8] is applied to the design data, considering an influent BOD concentration (M1) of 259 ± 58 mg·L⁻¹ and a target concentration of 60 mg·L⁻¹ according to Mexican regulations [48], making it possible to calculate a wetland area decrease of 27%.

4. Conclusions

Mean global efficiencies found for the complete system for the lower HRT (two days) were: 89.5% ± 4.4% for BOD, 84.2% ± 4.0% for COD, 32.5% ± 13.2% for total nitrogen (N_{tot}) and 43.8% ± 12.3% for total phosphorous (P_{tot}). Mean removal efficiencies for the higher HRT (four days), were 86.1% ± 3.1% for BOD, 81.7% ± 3.9% for COD, 32.9% ± 17.7% for N_{tot} and 30.2% ± 16.0% for P_{tot}. Finally, for the intermediary HRT (three days), the results were: 79.3% ± 8.7% for BOD, 85.6% ± 3.1% for COD, 30.0% ± 16.8% for N_{tot} and 24.2% ± 17.7% for P_{tot}. The best mean efficiencies reached in the UAF stage for COD, BOD, N_{tot} and P_{tot} were 79.8%, 76.1%, 23.2% and 35.4%, respectively, at the HRT1. The best removal for nitrogen in the HSSCW was reached with a detention time of three and four days, with the longer time allowing further progress in the nitrogen cycle. The HRT recommended for phosphorus removal for UAF is two days, while for HSSCW an HRT of at least three days is recommended. In other words, two days is adequate to remove organic matter, but when the objective is to remove organic matter and nutrients a three-day HRT is recommended. Moreover, it would be

interesting to test HRTs longer than four days for HSSCW and to conduct a more comprehensive investigation of the interactions on the support media.

The UAF was responsible for the organic matter reduction while nitrogen removal was performed by the HSSCW. The goal of reducing the land surface required by the wetland was achieved, since the organic matter removal by the UAF decreased the land requirements moderately, and could lessen early clogging in the constructed wetland.

Acknowledgments

The authors would like to thank to State Water Commission (Comisión Estatal del Agua, CEA-Jalisco) for its support during the experimental stage and to National Council of Science and Technology (Consejo Nacional de Ciencia y Tecnología, CONACYT) for the scholarship granted to student María de la Luz Merino Solís and the support of the Project 128209 (FOMIX CONACY-Veracruz). Also, a special thanks to MSc Leonel Hernández Mena for his constructive comments and to Dana Erickson and Walter Meyer for their linguistic contribution.

Author Contributions

López-López Alberto and de Anda José conceived and designed the project and also they contributed reagents, materials and analysis tools; Merino-Solís María L. and Villegas Edgardo performed the experiments during the monitoring stage and performed the data analysis. All the authors wrote the paper.

Conflicts of Interest

The authors declare no conflict of interest.

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